

**JEE MAIN ANSWER KEY & SOLUTIONS**

**SUBJECT :- PHYSICS**

**CLASS :- 11<sup>th</sup>**

**PAPER CODE :- CWT-12**

**CHAPTER :- KTG & THERMODYNAMICS**

**ANSWER KEY**

1.	(B)	2.	(A)	3.	(C)	4.	(B)	5.	(B)	6.	(A)	7.	(A)
8.	(C)	9.	(A)	10.	(A)	11.	(C)	12.	(C)	13.	(B)	14.	(D)
15.	(C)	16.	(C)	17.	(D)	18.	(C)	19.	(A)	20.	(D)	21.	159
22.	500	23.	2.5kJ	24.	300m	25.	7730	26.	72	27.	750	28.	2
29.	900	30.	20										

**SOLUTIONS**

1. (B)  
**Sol.** For adiabatic process  $dQ = 0$   
 $dQ = 0$   
 $\therefore dU + dW = 0$   
 or  $\frac{dW}{dU} = -1$

2. (A)  
**Sol.** Efficiency of all reversible cycles depends upon temperature of source and sink which will be different.

3. (C)  
**Sol.** Tr. K.E. =  $\frac{3}{2}nRT = \frac{3}{2}PV$   
 $\frac{E_{Tr}}{V} = \frac{3}{2}P$   
 $E = \frac{3}{2}PV$

4. (B)  
**Sol.** From the conservation of the energy we have ,  
 Initial internal energy = Dissociation energy + final internal energy  
 $\frac{5}{2} \times 4 \times 2 \times 500$   
 $= 2000 + \frac{3}{2} \times 2 \times 2 \times T' + \frac{5}{2} \times 3 \times 2 \times T'$   
 $T' = \frac{8000}{21} = 100 \text{ T}$   
 $T = 4$

5. (B)  
**Sol.**  $\Delta Q = M, S, \Delta T$   
 $= 100 \times 10^{-3} \times 4.184 \times 20$   
 $= 8.4 \times 10^3$   
 $\Delta Q = 8.4 \text{ kJ}, \quad \Delta W = 0$   
 $\Delta Q = \Delta u + \Delta W$   
 $\therefore \Delta u = 8.4 \text{ kJ.}$  **Ans.**

6. (A)  
**Sol.** From first law of thermodynamics,  
 $Q = \Delta U + W$   
 For path iaf,  
 $50 = \Delta U + 20$   
 $\therefore \Delta U = U_f - U_i = 30 \text{ cal}$   
 For path ibf,  
 or  $Q = \Delta U + W$   
 $W = Q - \Delta U$   
 $= 36 - 30 = 6 \text{ cal.}$

7. (A)  
**Sol.** According to Mayer's relation,  
 $C_p - C_v = \frac{R}{m} = \frac{R}{28}$

8. (C)  
**Sol.** Work does not characterize the thermodynamic state of matter, it is a path function gives only relationship between two quantities.

9. (A)  
**Sol.**  $\frac{dP}{P} = -\gamma \frac{dV}{V}$  (For adiabatic)  
 $0.5 = -1.4 \frac{dV}{V}$   
 $\therefore$  Volume decrease by 0.36%

10. (A)  
**Sol.** We know that for ideal gas  $\frac{V_1}{T_1} = \frac{V_2}{T_2}$   
 (at constant pressure)  
 $\Rightarrow T_2 = \frac{V_2}{V_1} \times T_1 = \frac{3V}{V} \times 273$   
 $= 3 \times 273 \text{ K}$   
 $\Rightarrow T_2 = 819 \text{ K} = 819 - 273$   
 $= 546^\circ\text{C}$

11. (C)  
**Sol.**  $\Delta U = Q = 1^2 \times 100 \times 5 \times 60 \text{ J} = 30 \text{ KJ}$

12. (C)

**Sol.**  $V_{av} = \sqrt{\frac{8KT}{\pi m}}$ , as  $T = \text{constant}$   
 $\therefore V_{av} = \text{constant}$

13. (B)

**Sol.**  $TV^{\gamma-1} = \text{constant}$

$$T_1 V_1^{5-1} = T_2 (32V_1)^{5-1}$$

$$\frac{T_2}{T_1} = \frac{1}{(32)^{2/5}} = \frac{1}{4}$$

$$\eta = 1 - \frac{T_2}{T_1} = 1 - \frac{1}{4} = \frac{3}{4}$$

14. (D)

**Sol.**  $dQ = dW + dU$   
 $dQ = PdV + dU$   
 $dQ = nRdT + dU$   
 $dQ = \frac{2dU}{f} + dU$

$$\frac{dU}{dQ} = \frac{1}{\left(\frac{2}{f} + 1\right)}$$

$$\frac{dU}{dQ} = \frac{5}{7}$$

15. (C)

**Sol.** Efficiency of the Carnot engine is given by

$$\eta = 1 - \frac{T_2}{T_1}$$

where  $T_1 = \text{temperature of source}$

$T_2 = \text{temperature of sink}$

Given  $\eta = 50\% = 0.5$ ,  $T_2 = 500 \text{ K}$

Substituting in relation (i), we have

$$0.5 = 1 - \frac{500}{T_1} \quad \text{or} \quad \frac{500}{T_1} = 0.5$$

$$\therefore T_1 = \frac{500}{0.5} = 1000 \text{ K}$$

Now, the temperature of sink is changed to  $T_2$  and the efficiency becomes 60% i.e., 0.6.

Using relation (i), we get

$$0.6 = 1 - \frac{T_2}{1000}$$

$$\text{or} \quad \frac{T_2}{1000} = 1 - 0.6 = 0.4 \quad \text{or}$$

$$T_2 = 0.4 \times 1000 = 400 \text{ K}$$

16. (C)

**Sol.**  $PV^\gamma = \text{constant}$

$$T_1 = 273 + 27 = 300 \text{ K}$$

$$P \left(\frac{T}{P}\right)^\gamma = \text{constant}$$

$$T_2 = 273 + 927 = 1200 \text{ K}$$

$$P^{1-\gamma} T^\gamma = \text{constant}$$

$$\Rightarrow P_1^{1-\gamma} T_1^\gamma = P_2^{1-\gamma} T_2^\gamma$$

$$\Rightarrow 2^{1-1.4} (300)^{1.4} = P_2^{1-1.4} (1200)^{1.4}$$

$$\Rightarrow \left(\frac{P_2}{P_1}\right)^{1-\gamma} = \left(\frac{T_1}{T_2}\right)^\gamma$$

$$\Rightarrow \frac{P_2}{P_1} = \left(\frac{T_1}{T_2}\right)^{\frac{\gamma}{1-\gamma}}$$

$$\left(\frac{P_1}{P_2}\right)^{1-\gamma} = \left(\frac{T_2}{T_1}\right)^\gamma$$

$$\left(\frac{P_1}{P_2}\right)^{1-1.4} = \left(\frac{1200}{300}\right)^{1.4}$$

$$\left(\frac{P_1}{P_2}\right)^{-0.4} = (4)^{1.4} \quad \left(\frac{P_2}{P_1}\right)^{0.4} = 4^{1.4}$$

$$P_2 = P_1 4^{\left(\frac{1.4}{0.4}\right)} = P_1 4^{\left(\frac{7}{2}\right)}$$

$$= P_1 (2^7) = 2 \times 128 = 256$$

17. (D)

**Sol.** The rms velocity of the molecule of a gas of molecular weight  $M$  at kelvin temperature  $T$  is given by,

$$C_{rms} = \sqrt{\left(\frac{3RT}{M}\right)}$$

Let  $M_O$  and  $M_H$  are molecular weights of oxygen and hydrogen and  $T_O$  and  $T_H$  the corresponding Kelvin temperature at which  $C_{rms}$  is same for both gases.

$$C_{rms(O)} = C_{rms(H)}$$

$$\sqrt{\left(\frac{3RT_O}{M_O}\right)} = \sqrt{\left(\frac{3RT_H}{M_H}\right)}$$

$$\text{Hence, } \frac{T_O}{M_O} = \frac{T_H}{M_H}$$

$$T_O = 273 + 47 = 320 \text{ K}$$

$$M_O = 32, M_H = 2$$

$$\therefore T_H = \frac{2}{32} \times 320 = 20 \text{ K}$$

18. (C)

**Sol.** Adiabatic Bulk modulus  $B = -V \frac{dP}{dV}$

$$= \gamma P = \gamma \frac{nRT}{V}$$

$$\therefore \frac{B_i}{B_f} = \frac{T_0}{V_0} \times \frac{V}{T} = \frac{T_0}{V_0} \times \frac{V_0/8}{4T_0} = \frac{1}{32}$$

19. (A)

**Sol.** Number of moles of He =  $\frac{1}{4}$

$$\text{Now } T_1 (5.6)^{\gamma-1} = T_2 (0.7)^{\gamma-1}$$

$$T_1 = T_2 \left(\frac{1}{8}\right)^{2/3}$$

$$4T_1 = T_2$$

$$\text{Work done} = -\frac{nR[T_2 - T_1]}{\gamma - 1}$$

$$= -\frac{1}{4} \frac{R[3T_1]}{\frac{2}{3}} = -\frac{9}{8} RT_1$$

20. (D)

**Sol.** 
$$\frac{v_{RMS_{He}}}{v_{RMS_{Ar}}} = \frac{\sqrt{\frac{3RT}{m_{He}}}}{\sqrt{\frac{3RT}{m_{Ar}}}}$$

$$= \sqrt{\frac{m_{Ar}}{m_{He}}} = \sqrt{\frac{40}{4}} = \sqrt{10} \approx 3.16$$

21. 159

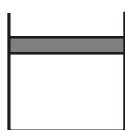
**Sol.**  $kl_0 = 10^5 \text{ A}$

$$\left(10^5 + \frac{kx}{A}\right) = P = \left(10^5 + \frac{l_0}{5A}\right) = 1.2 \times 10^5$$

$$V = V_0 + Ax = A(l_0 + x) = 1.2 V_0$$

$$= 1.2 A l_0 \Rightarrow x = \frac{l_0}{5A} \quad \frac{P_0 V_0}{T_0} = \frac{PV}{T}$$

$$T = \frac{PV}{P_0 V_0} T_0 = \frac{1.2 \times 10^5 \times 1.2 V_0}{10^5 \times V_0} \times 273$$



$$\Rightarrow 300 \times 1.44 = 432 \text{ K}$$

$$\Rightarrow T = 432 - 273 = 159 \text{ }^\circ\text{C}$$

22. 500

**Sol.**  $\frac{\text{Work done}}{\text{Total Heat given}} \times 100 = \eta$

$$W = \frac{50}{100} \times 1000 = 500 \text{ J}$$

23. 2.5 kJ

**Sol.**  $W_{\text{gas}} + W_{\text{spring}} + W_{\text{after}} = 0$

$$W_{\text{gas}} - \frac{1}{2} \times 25 \times 10^3 \times$$

$$(0.2)^2 - 10^5 \times 0.05 \times 0.4 = 0$$

$$W_{\text{gas}} = 2500 \text{ J} = 2.5 \text{ kJ}$$

24. 300 m/s

**Sol.** R.M.S. value for the four molecules is

$$= \sqrt{\frac{(100)^2 + (100)^2 + (300)^2 + (500)^2}{4}}$$

$$= 100 \sqrt{\frac{1+1+9+25}{4}} \text{ m/s}$$

$$= 300 \text{ m/s} \quad \text{Ans.]}$$

25. 7730 K

26. 72

**Sol.**  $(p_0 + h_{pg}) v_0 = (p_0 - h_{pg}) v$



$$(H + 8) \times 4 = (H - 8) \times 5$$

$$4H + 32 = 5H - 40$$

$$72 = H$$

27. 750

**Sol.**  $W = W_1 \left[ \frac{1 - (p_2 - p_0)^2}{(p_0 - p_1)^2} \right] \approx 750 \text{ J}$

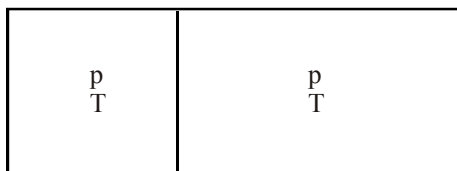
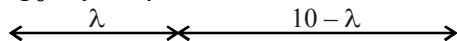
28. 2

Sol.  $PV_1 = n_1RT$

$$PA\ell = \frac{m}{32}RT$$

$$PA(10 - \ell) = \frac{m}{8}RT$$

$$\frac{\ell}{10 - \ell} = \frac{1}{4}$$



$$4\ell = 10 - \ell$$

$$\ell = 2 \text{ cm]$$

29. 900

Sol.  $(p_0 + 100) \times 400 = (p_0 - 100) \times 500$

$$100p_0 = 100 \times 900$$

$$p_0 = 900 \text{ m}$$

30. 20

Sol.  $p_i = p_0 + \frac{kx}{A} = 2 \times 10^5 \text{ P}$

$$p_f = 2 \times 10^5 + 10^6 x$$

$$v_i = 1A$$

$$v_f = (1 + x)A$$

$$\frac{PV}{T} = \text{const.}$$

$$\frac{2 \times 10^5 \times 1A}{T_0} = \frac{2 \times 10^5 + 10^6 x}{2T_0} \times (1 + x)A$$

$$2.4 = \frac{(2 + 10x)(1 + x)}{2}$$

$$2.4 = (1 + 5x)(1 + x)$$

$$2.4 = 1 + 5x^2 + 6x$$

$$5x^2 + 6x - 1.4 = 0$$

$$x = \frac{-6 + \sqrt{36 + 4 \times 5 \times 1.4}}{10} = 0.2 \text{ m} = 20 \text{ cm}$$

PE